



Environmental Management Division Environmental Control Services



Environmental Control Programs

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SOURCE TESTING FOR PARTICULATE
EMISSIONS FROM THE PATHOLOGICAL
INCINERATOR AT THE
SEVEN OAKS GENERAL HOSPITAL
WINNIPEG, MANITOBA
1986

Air Pollution Control
Environmental Control Services
Department of Environment
and Workplace Safety and Health

TABLE OF CONTENTS

	PAGE
LIST OF TABLES.....	ii
LIST OF FIGURES.....	iii
ABSTRACT.....	iv
INTRODUCTION.....	1
PROCESS DESCRIPTION.....	2
PROCESS SCHEDULE.....	6
OFFICIAL TESTS.....	7
RESULTS.....	11
DISCUSSION OF RESULTS.....	14
CONCLUSION.....	15
BIBLIOGRAPHY.....	16
APPENDIX 1 - MANITOBA REGULATION 334/74.....	17
APPENDIX 2 - VELOCITY PROFILES.....	19
APPENDIX 3 - EQUIPMENT CALIBRATION DATA.....	23
APPENDIX 4 - FIELD DATA SHEETS.....	27
APPENDIX 5 - LABORATORY ANALYSIS DATA.....	31

LIST OF TABLES

	PAGE
TABLE 1 - Incinerator Burn Cycle Sequence.....	5
TABLE 2 - Summary of Sampling Parameters for Particulate Tests.....	12
TABLE 3 - Particulate concentrations and Emission Rates.....	13

LIST OF FIGURES

	PAGE
FIGURE 1 - Plibrico CABP 450 Incinerator as Installed at Seven Oaks General Hospital.....	4
FIGURE 2 - Cross Section of Divided Stack.....	9
FIGURE 3 - Particulate Stack Sampling Train.....	10

ABSTRACT

After numerous reports of black smoke being emitted from the Seven Oaks General Hospital incinerator stack, the Air Pollution Control Section conducted a particulate source emission survey between April 22 and April 25, 1986.

During testing, the average particulate concentration was 0.409 grams per dry standard cubic meter at stack values of carbon dioxide (CO_2). When stack CO_2 concentration was corrected to 12%, the average particulate concentration increased to 0.751 grams per dry standard cubic meter calculated at standard* conditions.

This value exceeds Manitoba Incinerator Regulation, 334/74, Clause 3(1) (see Appendix 1). After incinerator and stack repairs or modifications have been completed a second emission survey will be required to demonstrate compliance.

* temperature 20°C, pressure 760 mm Hg

INTRODUCTION

A pathological incinerator was installed at the Seven Oaks General Hospital for the purpose of completely destroying Type I (general hospital rubbish) and Type IV (pathological waste). To determine general compliance with Manitoba Incinerator Regulation 334/74, Clause 3(1), the Air Pollution Control Section conducted three particulate tests between April 22 and April 25, 1986 on the exhaust stack while under normal operating conditions. Appendix 1 contains Manitoba Incinerator Regulation 334/74.

PROCESS DESCRIPTION

A Plibrico Model CABP 450 controlled air incinerator was tested for particulate emissions. Figure 1 depicts the incinerator as installed at the Seven Oaks General Hospital. The incinerator operates twice daily (12 hour cycle) on week days and once on the weekends to dispose of pathological and general hospital waste. The combined design capacity is 385 cubic feet of Type I (general hospital rubbish) and 100 pounds of Type IV waste (pathological) per 12 hour cycle.

The primary and after burner chambers were heated by natural gas burners. The maximum capacity of the ignition burner and reaction burner were 400,000 Btu/hr. and 1,500,000 Btu/hr. respectively. The incineration process was controlled automatically by a programmed timer which determined the sequence and duration of firing in the two chambers. Refer to Table 1 for burn cycle sequence during stack testing. Drying, ignition, and partial combustion of the waste occurred in the pathological and primary chambers. Air intake to the primary chambers was reduced to control the combustion rate and temperature. Final combustion of gasified and partially combusted volatile components occurred at the reaction burner (secondary chamber), where air was supplied in excess of stoichiometric requirements to ensure complete combustion.

The incinerator combustion products exit into a 117 foot divided stack which also serves the power boilers. The steel stack was designed with a 4 inch ceramic liner with a continuous interior

diameter of 45 inches. The 3 inch divider wall was located 19.5 inches from the incinerator side and 22.5 inches from the power boiler side.

At the end of the 12 hour cycle, the cooled ashes were removed from the primary and pathological chambers.

SEVEN OAKS GENERAL HOSPITAL

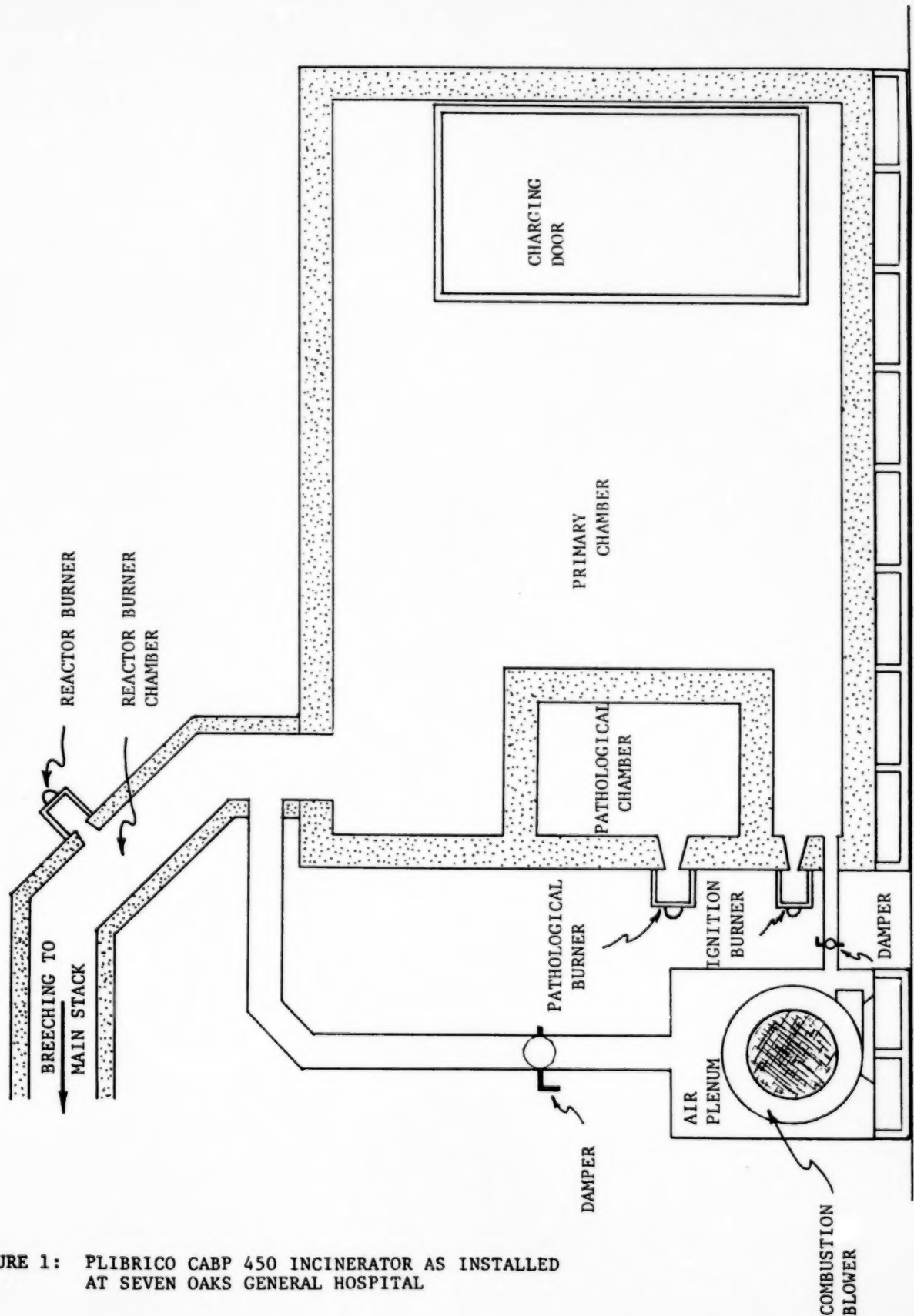


FIGURE 1: PLIBRICO CABP 450 INCINERATOR AS INSTALLED AT SEVEN OAKS GENERAL HOSPITAL

Table 1: INCINERATOR BURN CYCLE SEQUENCE

<u>CONTROL</u>	<u>TIME (HOURS:MINUTES)</u>
----------------	-----------------------------

CYCLE INITIATION	0:00*
REACTOR BURNER ON	0:01
COMBUSTION BLOWER ON	0:30
IGNITION BURNER ON	0:31
IGNITION BURNER OFF	0:52
PATHOLOGICAL BURNER ON	0:55
PATHOLOGICAL BURNER OFF	2:55
REACTOR BURNER OFF	4:01
COMBUSTION BLOWER OFF	12:01

* Start time is expressed as 0:00 hours for convenience only

PROCESS SCHEDULE

Charging wastes for the 1986 particulate emission survey consisted of:

- general hospital rubbish packed in green garbage bags.
- pathological waste packed in orange garbage bags.
- special wastes such as plastic tubing and syringes, glass ampules and out of date drugs.

The incinerator was charged pursuant to incinerator design and operating instructions.

OFFICIAL TEST

The sampling facility consisted of a portable platform which permitted access to the northeast stack port and supported the sample probe and recovery train while sampling operations were in progress at roof level.

The height of the 45 inch inside diameter divided stack was approximately 55 feet from the breeching to the sampling ports which translates into 14.7 stack diameters of undisturbed flow. Two sample ports were installed on the divided stack but due to divider deterioration it was decided no greater accuracy could be achieved by sampling both ports. Figure 2 shows the location of the three sampling points and the two sampling ports. The northeast sample port was used for the three test survey. Sampling intervals were 5 minutes per point and each point was sampled twice.

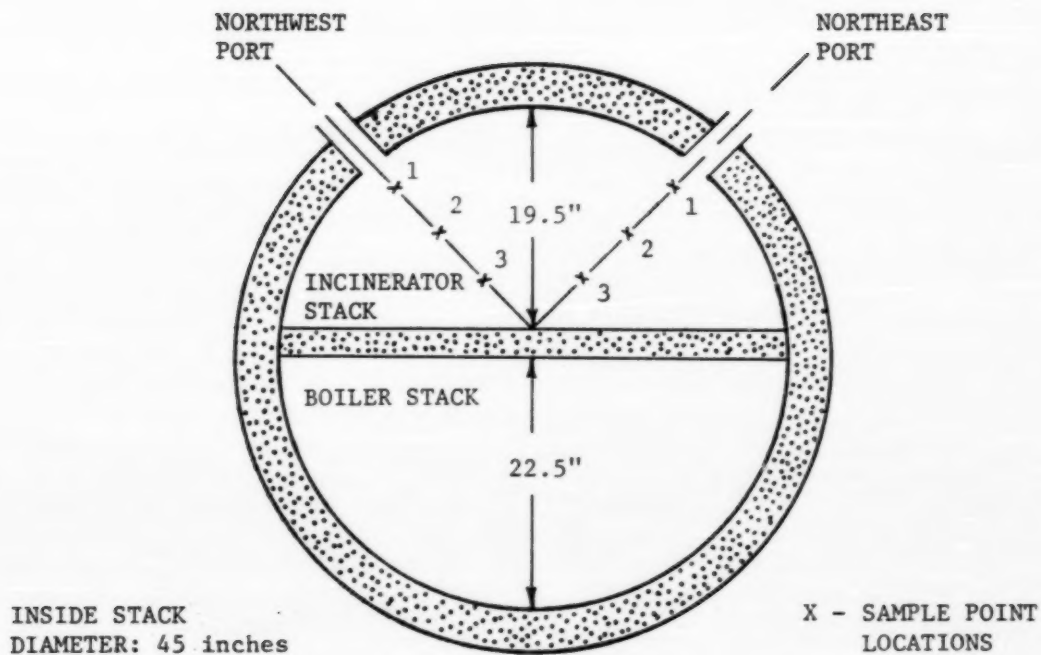
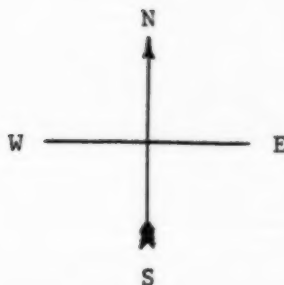
Particulate testing was conducted according to EPS method E, with sample probe modifications to compensate for the elevated stack temperature. Figure 3 depicts the sample collection system. The particulate was drawn into a stainless steel sample nozzle and through a water cooled stainless steel probe. Connected to the probe was a miniature cyclone and flask which collected particulate matter greater than 10 μ diameter. The sample was then passed through a Whatman 934 AH glass fiber filter supported by a porous fritted glass disc which removed particulates of 0.3 μ diameter and greater. Both the cyclone and the filter were heated to prevent moisture condensing on glassware in the hot box. The gas sample was then passed through four

500 ml Greenburg-Smith impingers connected in series. The first, second and fourth impingers utilized modified straight tips while the second impinger was of Standard Greenburg-Smith design. The first and second impingers were both filled with 100 mls of deionized water. The third impinger was initially empty while the fourth was filled with 200 grams of indicating silica gel which removed remaining moisture from the gas sample. For each test the impingers were immersed in an ice bath to condense water contained in the stack gas sample.

A Bendix Series 4500 Isokinetic Stack Sampler was used to extract the sample from the stack. Gas velocity in the stack was measured with a S-type pitot tube and a Dwyer Magnehelic Differential Pressure gauge (range 0-0.25 inches water). Velocity profiles for all tests can be found in Appendix 2. Dry gas meter and pitot tube calibration sheets are presented in Appendix 3. A Hays-Republic Model 621A Gas Analyzer was used to determine CO_2 (carbon dioxide), O_2 (oxygen) and CO (carbon monoxide) content of the stack gas, while N_2 (nitrogen) was calculated by difference. Stack temperature was measured by a K type thermocouple.

After sample recovery from the stack train, samples were submitted to the W. M. Ward Technical Services Laboratory, 745 Logan Avenue, for gravimetric analysis of particulate.

SEVEN OAKS GENERAL HOSPITAL



TRAVERSE POINT LOCATION FROM STACK WALL	
TRAVERSE POINT	DISTANCE inches
1	1.98
2	6.62
3	13.28

FIGURE 2: CROSS SECTION OF DIVIDED STACK

RESULTS

The Seven Oaks General Hospital pathological incinerator was operated normally during particulate tests. Sampling parameters are summarized in Table 2. Appendix 4 contains field data sheets.

Particulate concentrations and emission rates are summarized in Table 3. Laboratory analytical reports are located in Appendix 5.

SEVEN OAKS GENERAL HOSPITAL

TABLE 2: SUMMARY OF SAMPLING PARAMETERS FOR PARTICULATE TESTS

TEST NUMBER	1	2	3	AVERAGE
Sampling Date	APRIL 22, 1986	APRIL 23, 1986	APRIL 25, 1987	-
Sampling Time	12:04 P.M. 12:34 P.M.	11:00 A.M. 11:30 A.M.	10:30 A.M. 11:00 A.M.	-
Sampling Duration min	30	30	30	-
Average Stack Gas Temperature °F (°C)	1026 (552)	892 (478)	851 (455)	923 (495)
Ambient Temperature °F (°C)	51 (11)	66 (19)	46 (8)	54 (13)
Average Stack Gas Velocity ft/sec. (m/s)	21.2 (6.5)	18.6 (5.7)	21.1 (6.4)	20.3 (6.2)
Stack Gas Static Pressure inches H ₂ O (mmH ₂ O)	0.42 (10.7)	0.42 (10.7)	0.42 (10.7)	0.42 (10.7)
Stack Gas Moisture %	8.4	10.8	9.8	9.7
Stack Gas Composition % By Volume on a Dry Basis	N ₂	81.7	82.7	82.2
	O ₂	11.3	10.8	11.5
	CO ₂	7.0	6.5	6.3
	CO	-	-	-
Sample Volume acf (acm)	16.908 (0.4788)	17.376 (0.4921)	19.136 (0.5419)	17.807 (0.5043)
Average Gas Meter Temperature °F (°C)	84 (29)	87 (31)	82 (28)	84 (29)
Average Orifice Pressure Drop inches H ₂ O (mmH ₂ O)	1.110 (28.2)	1.164 (29.6)	1.462 (37.1)	1.245 (31.6)
Average Isokinetic Factor %	99.4	108.4	100.3	102.7

SEVEN OAKS GENERAL HOSPITAL

TABLE 3: PARTICULATE CONCENTRATIONS AND EMISSION RATES

TEST NUMBER	1	2	3	AVERAGE
Sampling Volume dscm	0.4713	0.4627	0.5207	0.4849
Total Particulate Catch mg	179.1	124.6	301.5	201.7
Average Stack Gas Volumetric Flow Rate dscm/hr	8,503	7,653	9,256	8,471
*Particulate Emission at Stack Values of CO ₂ grams/dscm	0.380	0.269	0.579	0.409
Particulate Emission Corrected to 12% CO ₂ grams/dscm	0.651	0.497	1.112	0.753
Particulate Emission Rate at Stack Value of CO ₂ kg/hr	3.2	2.1	5.4	3.6

* Particulate emissions are calculated on a dry basis at standard conditions. That is, a temperature of 20°C centigrade (68° fahrenheit) and a pressure of 760 mm Hg (29.92 in. Hg) as stated in Section 1(j) of Manitoba Incinerator Regulation 334/74.

DISCUSSION OF RESULTS

The Seven Oaks General Hospital is equipped with a divided stack which serves the power boiler and the incinerator. An incinerator particulate emission survey was conducted through the northwest port. A preliminary velocity traverse indicated that no additional accuracy could be achieved by sampling through both ports due to the present condition of the stack. Stack diameter measurements revealed erosion of the ceramic stack liner increasing the inside stack diameter from 45 inches to 47 inches. At the time of the survey it was discovered the wall which separated the power boiler and the incinerator stack did not exist at various locations including the vicinity where sample ports were located. Therefore incinerator and power boiler exhaust gases were mixed as they travelled up the stack. This condition presented several problems. The incinerator exhaust was diluted by the boiler exhaust decreasing the percent carbon dioxide in the flue gas. Final combustion of the gasified and partially combusted volatile components occurred in the reaction burner chamber. The stack temperature was decreased when the two exhaust gases mixed, shorting the high temperature retention time created by the reaction burner, resulting in increased particulate emissions. Stack repairs will be required before additional testing can be carried out.

CONCLUSION

Tests 1 to 3 indicated an average particulate emission of 0.753 grams/dscm when corrected to 12% CO₂ (0.409 grams/dscm at average stack value of CO₂), which is in non-compliance with Manitoba Incinerator Regulation 334/74, Section 3(1) limit of 0.23 grams/dscm of flue gas corrected to 12% CO₂.

BIBLIOGRAPHY

1. Standard Reference Method For Source Testing: Measurements of Emissions of Particulates From Stationary Sources.
Ottawa, Ontario: Environment Canada, Environmental Protection Service, 1974 (Report EPS 1-AP-74-1).

- 17 -

APPENDIX 1

MANITOBA REGULATION 334/74

Manitoba Regulation 334/74

Being a Regulation Under The Clean Environment Act
Respecting Incinerators

(Filed December 31, 1974)

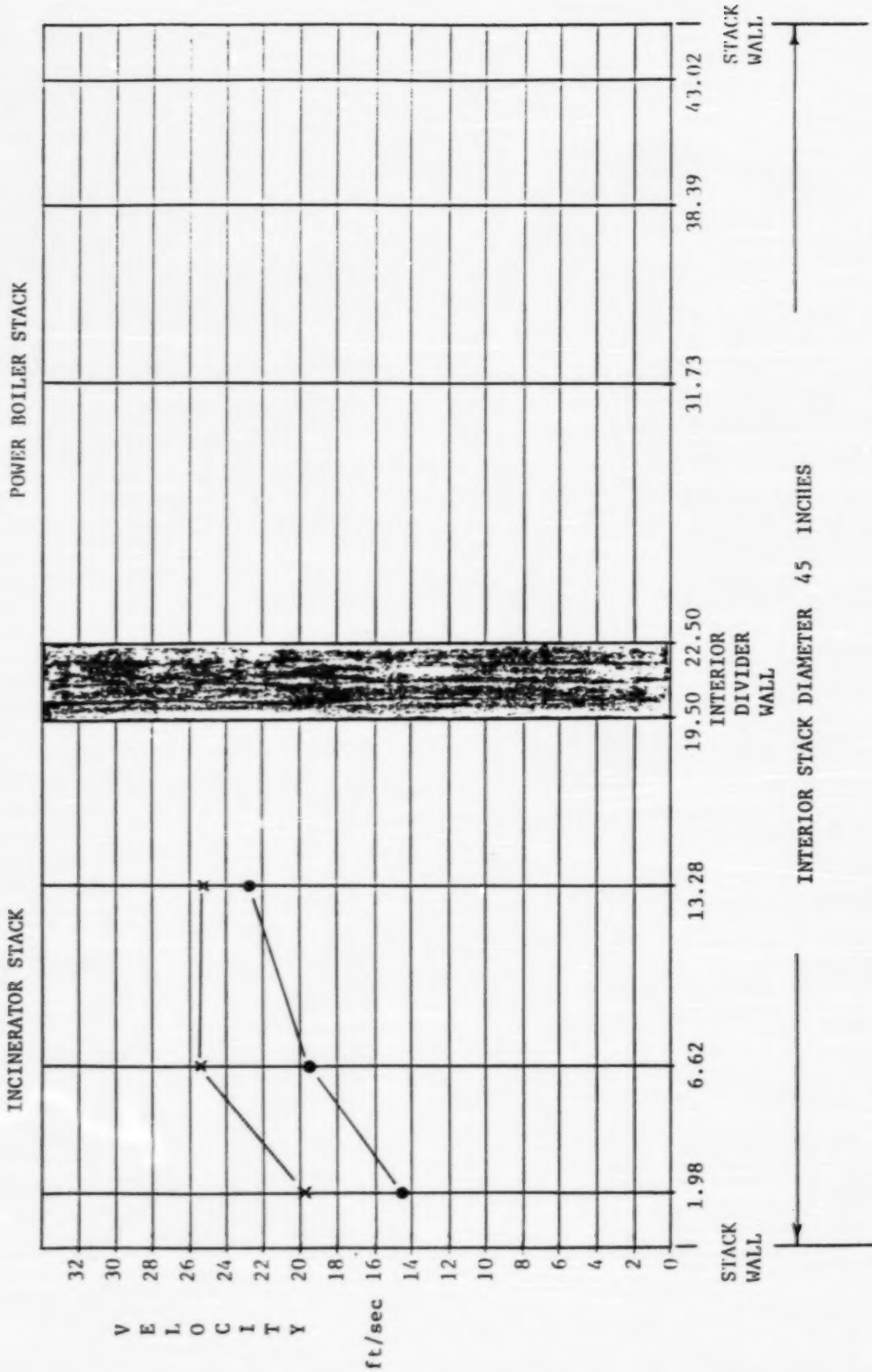
1 In this Regulation,

- (a) "domestic incinerator" means an incinerator used for a single family residence or for a two-family residence, either in duplex or double house form, or for multiple-dwelling units in which such incinerator serves fewer than three apartments;
- (b) "existing incinerator" means an incinerator placed in operation before the effective date of this Regulation;
- (c) "flue-fed incinerator" means an incinerator provided with a flue which serves as a charging chute in addition to conducting the products of combustion to the atmosphere;
- (d) "incinerator" means a device used for the process of burning waste and from which the products of combustion are conveyed to the atmosphere by passage through a stack;
- (e) "new incinerator" means an incinerator placed in operation after the effective date of this Regulation;
- (f) "opacity" means the degree to which emissions reduce the transmission of light and obscure the view of an object in the background;
- (g) "particulates" means any material, except uncombined water, which exists in a finely divided form as a liquid or solid at standard conditions;
- (h) "Ringelmann Number" means a value on the Ringelmann Smoke Chart for grading the density of smoke published by the U.S. Bureau of Mines, or any other chart, recorder, indicator or device for the measurement of smoke density which is approved by the Department as the equivalent of the said Ringelmann Smoke Chart;
- (i) "smoke" means small gas-borne particles resulting from combustion, consisting predominantly but not exclusively of carbon and ash, which form a visible plume under draft;
- (j) "standard condition" means a temperature of 20° Centigrade (68° Fahrenheit) and a pressure of 760 mm Hg (29.92 in. Hg);
- (k) "standard cubic foot" means the volume of one cubic foot of gas at standard conditions;
- (l) "standard cubic metre" means the volume of one cubic metre of gas at standard conditions.

- 2(1)** A person intending to construct or set into operation a new incinerator is not required to file a proposal with the Department as provided in Section 14(1) of The Clean Environment Act.
- 2(2)** Prior to operating a new incinerator a person shall register the incinerator with the Department on a form approved by the Department.
- 3(1)** No person shall operate any new incinerator which emits more than 0.23 grams of particulates per standard cubic metre (0.10 grains per standard cubic foot) of dry flue gas corrected to 12 percent carbon dioxide by volume.
- 3(2)** No person shall operate a new incinerator which emits smoke the opacity of which is equal to or greater than
- (a) 40 percent (equivalent to number 2 on the Ringelmann Smoke Chart) at any time; or
 - (b) 20 percent (equivalent to number 1 on the Ringelmann Smoke Chart) for a period exceeding 4 minutes in any one hour.
- 4(1)** No person shall construct or install any domestic incinerator after the effective date of this Regulation.
- 4(2)** No person shall construct or install any flue-fed incinerator after the effective date of this Regulation.
- 5(1)** The rated capacity and the type of waste material for which the incinerator is designed shall be displayed in a conspicuous location near the incinerator.
- 5(2)** Detailed instructions for the operation of the incinerator shall be posted in a conspicuous location near the incinerator.
- 5(3)** Sampling ports shall be suitably located in the stack or breeching of new incinerators.
- 6** The method for measurement of particulates and opacity of smoke from incinerators shall be as approved by the Department.

APPENDIX 2
VELOCITY PROFILES

TEST NO. 1
 NORTH EAST PORT
 WIND SPEED 50 mph
 DIRECTION SOUTH
 COMBINED STACK
 INCINERATOR STACK
 FIRST PASS x
 SECOND PASS ●



SEVEN OAKS GENERAL HOSPITAL,
INCINERATOR STACK VELOCITY PROFILE

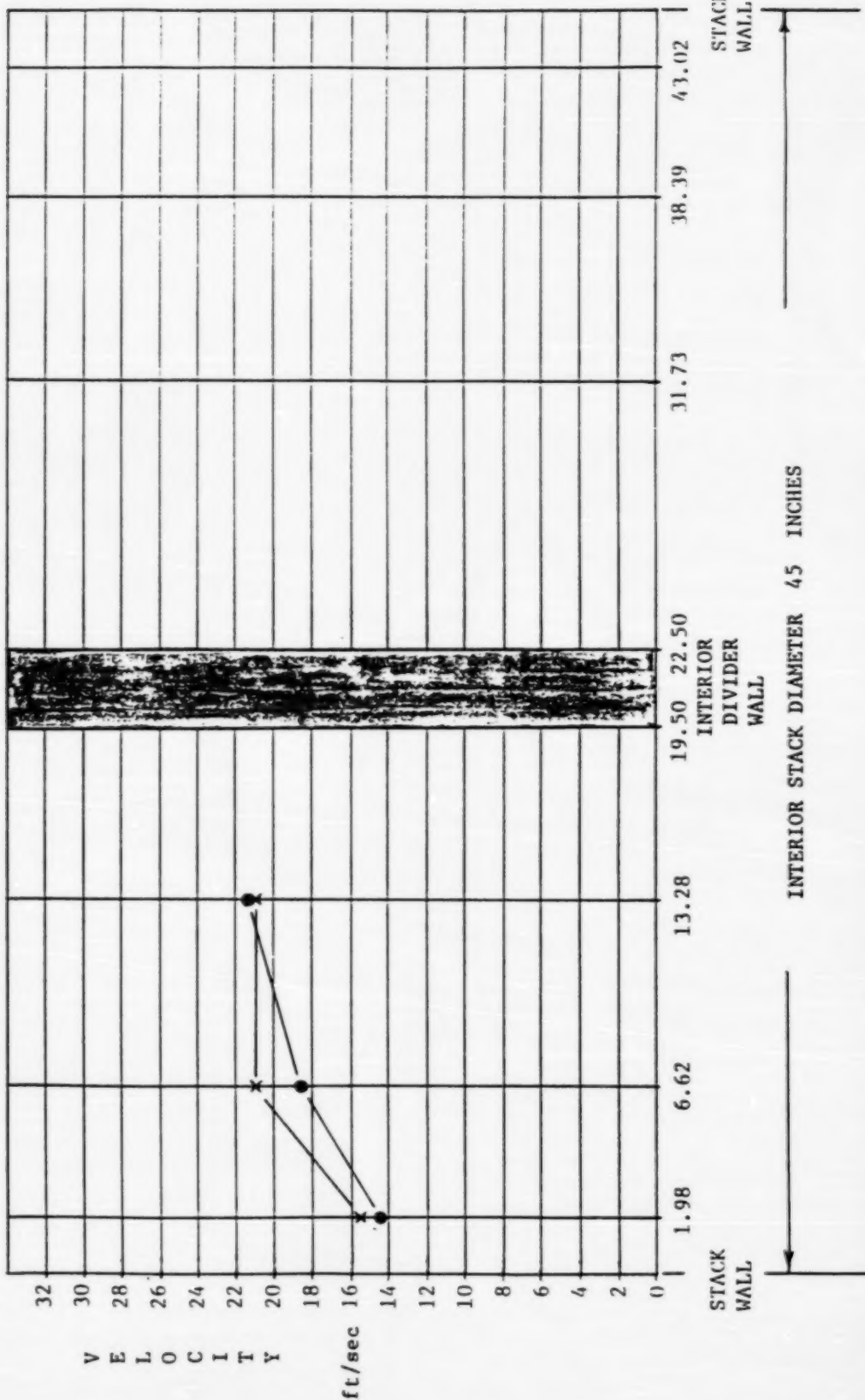
TEST NO. 2
NORTH EAST PORT
FIRST PASS x
SECOND PASS •

WIND SPEED
40 mph
DIRECTION
SOUTH

COMBINED STACK

INCINERATOR STACK

POWER BOILER STACK



INCINERATOR STACK VELOCITY PROFILE

TEST NO. 3

NORTH EAST PORT

FIRST PASS x

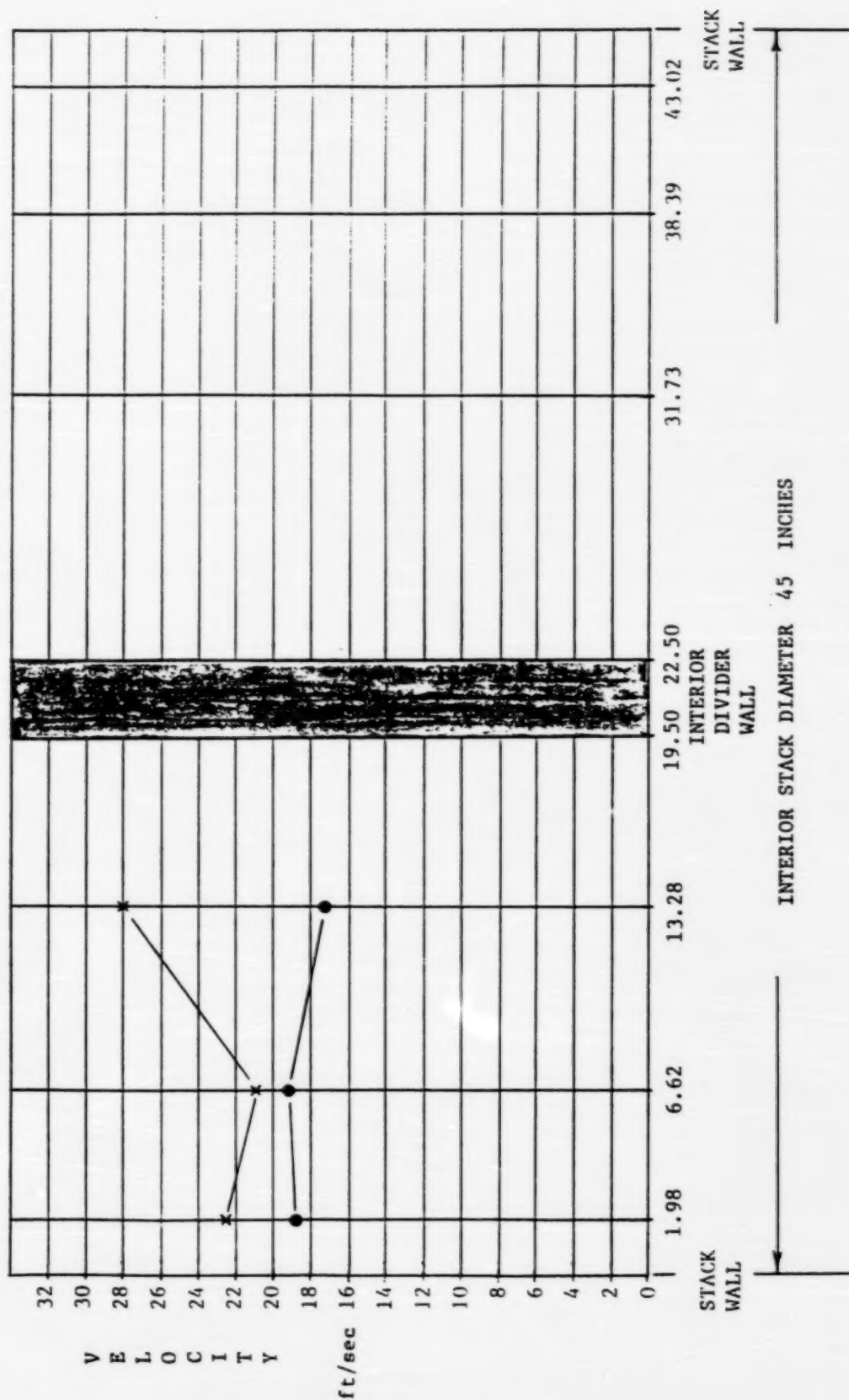
SECOND PASS ●

WIND SPEED 30 mph
DIRECTION SOUTH EAST

COMBINED STACK

INCINERATOR STACK

POWER BOILER STACK



APPENDIX 3
EQUIPMENT CALIBRATION DATA

S-TYPE PITOT TUBE CALIBRATION

PROBE SIZE (ft) 5 CALIBRATION # 86-24
 PROBE LINER S.S. WATER COOLED DATE APRIL 10, 1986
 PROBE MANUFACTURER BAROMETRIC PRESSURE (Hg) 29.06
 TIP SIZE (inches) 0.500 AMBIENT TEMP. (°C) 22.4
 TIP TYPE S.S OPERATOR KR. + A.S.
 STACK THERMOCOUPLE ☒ PRESENT
☐ ABSENT

HP 97 INPUT/OUTPUT

Temp	<u>22.4</u>	°C	4.	<u>0.46</u>	Δp (std)	8.	<u>1.32</u>	Δp (std)
Bar. Press	<u>29.06</u>	In. Hg		<u>14.531098</u>			<u>24.615376</u>	
Scale Factor	<u>0.1</u>			<u>0.72</u>	Δp (s-pitot)		<u>2.12</u>	Δp (s-pitot)
				<u>0.797307</u>			<u>0.787104</u>	
				<u>14.534143</u>			<u>24.620534</u>	

1.	<u>0.10</u>	Δp (std)	5.	<u>0.62</u>	Δp (std)	9.	<u>1.85</u>	Δp (std)
Tunnel Velocity	<u>6.77519</u>	ft/sec		<u>16.870010</u>			<u>29.141061</u>	
	<u>0.16</u>	Δp (s-pitot)		<u>1.00</u>	Δp (s-pitot)		<u>2.94</u>	Δp (s-pitot)
Cp, at this	<u>0.788593</u>	velocity		<u>0.785432</u>			<u>0.791271</u>	
Tunnel Velocity	<u>6.776579</u>	(using Cp)		<u>16.873546</u>			<u>29.147169</u>	

2.	<u>0.20</u>	Δp (std)	6.	<u>0.80</u>	Δp (std)		<u>0.790583</u>	Cp (ave)
	<u>9.581522</u>			<u>19.163044</u>			<u>0.007881</u>	Std. Dev.
	<u>0.31</u>	Δp (s-pitot)		<u>1.25</u>	Δp (s-pitot)		<u>8</u>	Deg. of Freedom
	<u>0.801211</u>			<u>0.798000</u>				
	<u>9.583530</u>			<u>19.167060</u>				

3.	<u>0.32</u>	Δp (std)	7.	<u>1.12</u>	Δp (std)		<u>2.306</u>	τ .05
	<u>12.119773</u>			<u>22.674019</u>			<u>0.784526</u>	Low Cp
	<u>0.53</u>	Δp (s-pitot)		<u>1.78</u>	Δp (s-pitot)		<u>0.790583</u>	Mean Cp
	<u>0.775086</u>			<u>0.791247</u>			<u>0.796641</u>	High Cp
	<u>12.122313</u>			<u>22.678771</u>				

1/2

DRY GAS METER & ORIFICE METER CALIBRATION SHEET

Dry Gas Meter S/N Read 711630
 Atmospheric Pressure 29.13 in. Hg / 740.0 mm Hg
 Ambient Temperature 23.0 °C

Lab No. 5618
 Calibrated re Large Wet Test Meter
 Calibrated by John P. Knapik & Kevin Brown
 Date 11 April 81

Orifice ΔH (in. H ₂ O)	W.T.M. Volume V _W (ft. ³)	Dry Gas Meter Reading		Temperature		Time t		W.T.M. Manometer Δm (in. H ₂ O)	Partial Pressure P _s (mm. Hg)	W.T.M. D.G.M. Ratio γ (—)	Flowrate Q _{sc} (ft. ³ /min.)
		Initial (ft. ³)	Final (ft. ³)	D.G.M. TV	D.G.M. T _i (°F.)	To (°F.)	(Min.:Sec.)				
0.500	4.0	275.706	282.756	4.058	14.5	18.1	10:29:30	0.30	15.575	1.0197	0.3572
0.500	4.0	283.719	288.032	4.014	14.8	18.2	10:30:43	0.27	15.673	1.0178	0.3862
0.500	4.0	289.047	293.121	4.077	15.0	18.3	10:31:48	0.28	15.772	1.0149	0.3861
1.03	4.0	296.170	300.288	4.078	15.1	18.4	7:17:77	0.34	15.871	1.0133	0.5534
1.03	4.0	302.338	306.451	4.113	15.2	18.4	7:20:11	0.35	15.871	1.0103	0.5538
1.03	4.0	307.472	311.587	4.115	15.3	18.5	7:20:20	0.46	15.771	1.0072	0.5534
1.52	5.0	314.671	319.820	5.233	15.5	18.6	7:27:89	0.53	16.071	0.9710	0.6786
1.53	5.0	320.842	325.994	5.174	15.5	18.6	7:28:07	0.56	16.071	1.0031	0.6794
1.53	5.0	327.022	332.157	5.147	15.5	18.7	7:28:15	0.51	16.071	1.0093	0.6794
2.05	6.0	334.225	340.406	6.237	15.6	18.7	7:40:98	0.59	16.172	0.9786	0.7777
2.05	6.0	341.439	347.625	6.186	15.7	18.7	7:41:02	0.47	16.172	1.0067	0.7777
2.05	6.0	348.652	354.837	6.185	15.7	18.7	7:41:12	0.47	16.172	1.0071	0.7777

Linear Regression: Intercept (b) 0.0086
 Slope (%) 0.659
 Coefficient of Determination (r²) 0.9995
 $\bar{\gamma} = 1.0094 \pm 0.0068$
 $\Delta H_o = 2.0725$

Comments:

DRY GAS METER & ORIFICE WATER CALIBRATION SHEET

Dry Gas Meter S/N: Borden 711030 Lab No. 5668
 Atmospheric Pressure 29.13 in. Hg / 740.0 mm Hg Calibrated re Large Wet Test Meter
 Ambient Temperature 23.0 °C Calibrated by Samuel K. Kuehner & Kuehner
 Date 11 April 56

Manometer Coefficient ΔH in. H ₂ O	W.T.M. Volume V _W (Ft. ³)	Dry Gas Meter Reading		D.G.M. Volume V _d (Ft. ³)	Temperature				Time t		W.T.M. Manometer Δh (in. H ₂ O)	Partial Pressure P _s (mm. Hg)	W.T.M. to G.M. Ratio γ (—)	 (—)	Flowrate Q S.S.F. Gm (Ft. ³ /min.)	
		Initial (Ft. ³)	Final (Ft. ³)		W.T.M. T _W (°F.)	D.G.M.		(Min.)	(Min.:Sec.)							
						T _i (°F.)	T _o (°F.)									
										(°C.)						(°F.)
3.06	6.0	311.114	372.34	61.77	66.0	18.9	116	89	2.28.26	6.4710	16.375	1.0612		1.4660	0.9374	
3.05	6.0	372.37	433.54	61.70	66.0	18.9	116	89	1.28.24	6.4707	16.375	1.0612		1.4937	0.9373	
3.04	6.0	396.582	457.752	61.70	66.0	18.9	117	89	1.28.27	6.4712	16.375	1.0613		1.4614	0.9374	
2.54	6.0	388.811	449.972	61.91	66.0	18.9	116	89	7.03.39	7.0563	16.375	1.0674		1.2818	0.8612	
2.54	6.0	371.022	402.200	61.78	66.1	18.9	116	89	7.03.37	7.0562	16.375	1.0675		1.2819	0.8609	
2.53	1.0	404.241	410.438	6.178	66.1	18.9	116	89	7.03.40	7.0567	16.375	1.0679		1.2793	0.8610	
0.497	4.0	442.485	446.593	4.105	66.5	19.2	119	88	10.40.74	10.6770	16.375	1.0614		0.5679	0.3903	
0.491	4.0	442.231	442.718	4.097	66.5	19.2	119	87	10.40.63	10.6772	16.375	1.0614		0.5640	0.3795	
0.491	4.0	442.715	442.838	4.093	66.7	19.3	117	87	10.40.67	10.6779	16.370	1.0170		0.5640	0.3794	

Linear Regression: Intercept (b) 0.0036 $\bar{\gamma}$ = 1.0094 ± 0.0063
 Slope (a) 0.6659 ΔH =
 Coefficient of Determination (r²) 0.9995

Comments:

APPENDIX 4
FIELD DATA SHEETS

FIELD DATA SHEET

Plant SEVEN OAKS GENERAL HOSPITAL

Location 2300 McPhillips Street, Winnipeg

Stack INCINERATOR STACK

Test number 1 Date April 22, 1986

Ambient temperature (°F) 51 Barometric pressure (in. Hg) 29.87 Time 12:04 P.M. - 12:34 P.M.

Nozzle diameter (in.) 0.498 Probe length/type 5 Foot/Stainless Steel Water Stack static pressure (in. H₂O) 0.42

Probe temperature (°F) - Filter holder temperature (°F) 240 Cooled Leak check 0.001 CFM @ 15 " Hg Vacuum

Traverse point number NORTH EAST PORT	Clock time	Stack gas temperature, °F	Gas meter volume, cu. ft.	Velocity pressure, in. H ₂ O	Orifice pressure drop in. H ₂ O	Gas meter temperature, °F Inlet Outlet	Final Impinger Temperature, °F	Pump vacuum in. H ₂ O	Isokinetic factor, %
1	5	1035	2.649	0.050	0.975	76	72	5	101.1
2	10	1131	3.157	0.076	1.390	89	73	6	99.7
3	15	1138	3.148	0.075	1.360	96	74	6	99.5
3	20	1044	3.034	0.064	1.240	100	74	6	100.6
2	25	967	2.722	0.050	1.020	102	75	5	98.8
1	30	838	2.198	0.031	0.682	102	76	5	96.9
Average or total	30	1026	16.908	0.058	1.110	94	74	6	99.4

FIELD DATA SHEET

Plant SEVEN OAKS GENERAL HOSPITAL Location 2300 McPhillips Street, Winnipeg Date April 23, 1986
 Stack INCINERATOR STACK Test number 2
 Ambient temperature ($^{\circ}\text{F}$) 66 Barometric pressure (in. Hg) 28.63 Time 11:00 A.M. - 11:30 A.M.
 Nozzle diameter (in.) 0.498 Probe length/type 5 Foot/Stainless Steel Water Cooled Stack static pressure (in. H₂O) 0.42
 Probe temperature ($^{\circ}\text{F}$) - Filter holder temperature ($^{\circ}\text{F}$) 290 Leak check 0.000 CFM @ 15" Hg Vacuum

Traverse point number	Clock time	Stack gas temperature, $^{\circ}\text{F}$	Gas meter volume, cu. ft.	Velocity pressure, in. H ₂ O	Orifice pressure drop in. H ₂ O	Gas meter temperature, $^{\circ}\text{F}$	Inlet	Outlet	Final impinger Temperature, $^{\circ}\text{F}$	Pump vacuum in. H ₂ O	Isokinetic factor, %
NORTH											
EAST PORT											
1	5	846	2.547	0.034	0.896		81	74	48	4	108.8
2	10	922	3.126	0.055	1.380		94	74	46	5	107.4
3	15	926	3.174	0.056	1.400		98	74	49	6	107.9
3	20	925	3.236	0.057	1.420		103	75	50	6	108.3
2	25	898	2.945	0.045	1.140		105	76	51	5	109.8
1	30	836	2.348	0.028	0.746		104	76	54	4	108.2
Average or total	30	892	17.376	0.046	1.164		98	75	50	5	108.4

FIELD DATA SHEET

- 30 -

Plant SEVEN OAKS GENERAL HOSPITAL Location 2300 McPhillips Street, Winnipeg
 Stack INCINERATOR STACK Test number 3 Date April 25, 1986
 Ambient temperature ($^{\circ}\text{F}$) 46 Barometric pressure (in. Hg) 29.27 Time 10:30 A.M. - 11:00 A.M.
 Nozzle diameter (in.) 0.498 Probe length/type 5 Foot/Stainless Steel Water Cooled Stack static pressure (in. H_2O) 0.42
 Probe temperature ($^{\circ}\text{F}$) - Filter holder temperature ($^{\circ}\text{F}$) 265 Leak check 0.000 CFM @ 15 " Hg Vacuum

Traverse point number NORTH EAST PORT	Clock time	Stack gas temperature, $^{\circ}\text{F}$	Gas meter volume, cu. ft.	Velocity pressure, in. H_2O	Orifice pressure drop in. H_2O	Gas meter temperature, $^{\circ}\text{F}$ Inlet Outlet	Final impinger Temperature, $^{\circ}\text{F}$	Pump vacuum in. H_2O	Isokinetic factor, %
1	5	810	3.416	0.071	1.670	72 69	40	7	100.2
2	10	936	2.975	0.057	1.230	88 70	42	12	101.0
3	15	860	4.177	0.108	2.505	92 71	43	12	99.9
3	20	919	2.509	0.039	0.855	97 72	44	5	101.1
2	25	852	2.868	0.050	1.100	100 73	43	5	99.2
1	30	727	3.191	0.055	1.410	102 76	44	6	100.1
Average or total	30	851	19.136	0.063	1.462	92 72	43	8	100.3

APPENDIX 5

LABORATORY ANALYSIS DATA

Date Sampled: 8.6.04 2.3
Date Recieved: 8.6.04 2.5

Date Sampled: 8.6.04

[illegible]

